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Studies of membrane scaling during water desalination by membrane distillation

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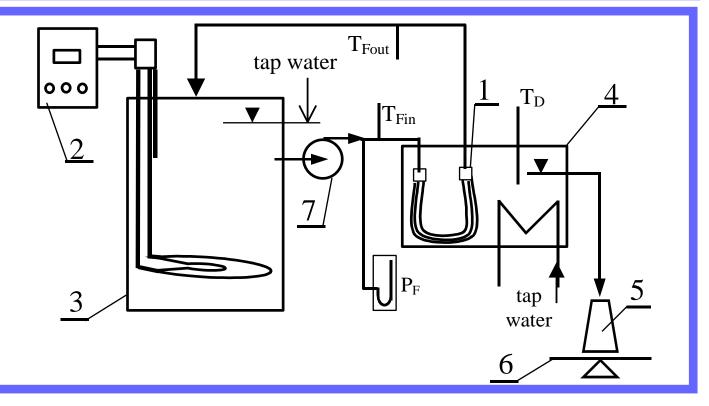
INTRODUCTION

In the case of MD carried out with natural water, the salts present in such water are retained and produced distillate is demineralized water. A major problem that hinders an industrial implementation of MD is a phenomenon of membrane wetting, which is often induced by membrane scaling

EXPERIMENTAL

The applied polypropylene membranes (Accurel PP S6/2, Membrana GmbH) have pore sizes with a nominal and maximum diameter of 0.2 μ m and 0.6 μ m, respectively, and porosity of 73%.

Fig. 1. DCMD experimental set-up. 1 – MD module, 2 – Nűga temperature regulator, 3 – feed tank, 4 – cooled distillate tank,
5 – distillate collector, 6 – balance, 7 – pump,
P_F – manometer, T_{Fin}, T_{Fout}, T_D– thermometer (notation: F – feed, D – distillate, in – input, out – output



RESULTS

The membrane modules were supplied with the feed preheated to a temperature 313 K and 333 K. The yield

obtained for these temperatures was 2.8 and 9.7 L/m²h, respectively (Figs 2 and 3). Low values of electrical conductivity of obtained distillates indicated, that the membranes were non-wetted during MD proces.

The changes of ions concentration in the feed were presented in Fig.4. Water demineralization by MD was carried out for 1400 h without module cleaning. However, the membrane scaling was confirmed by SEM examination of membrane samples (Figs 5 and 6).

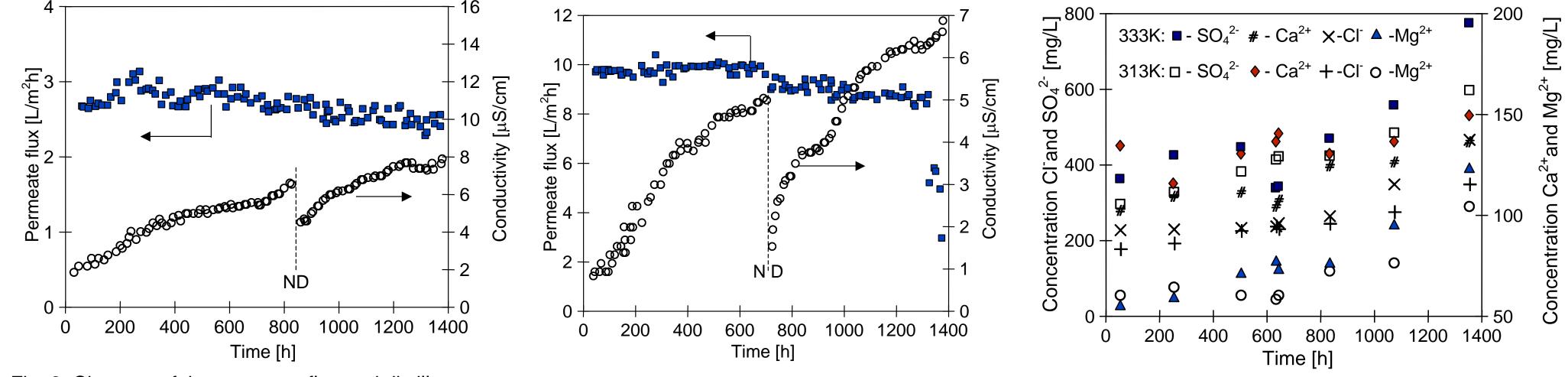
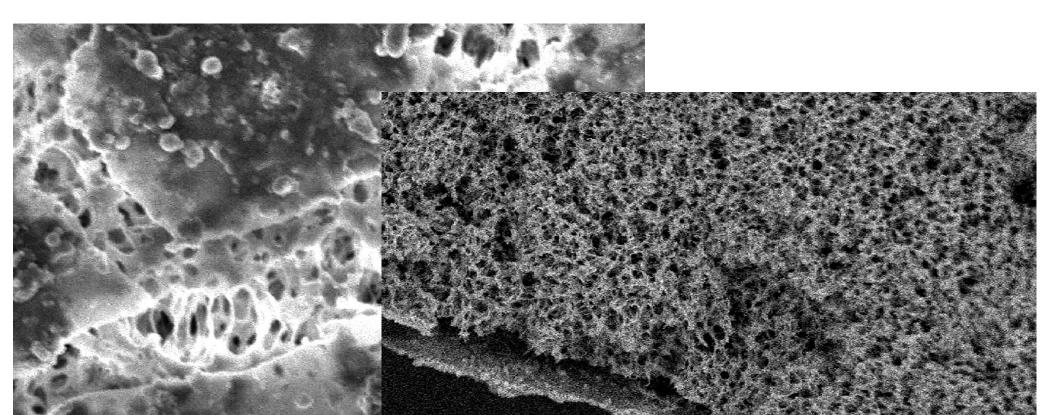
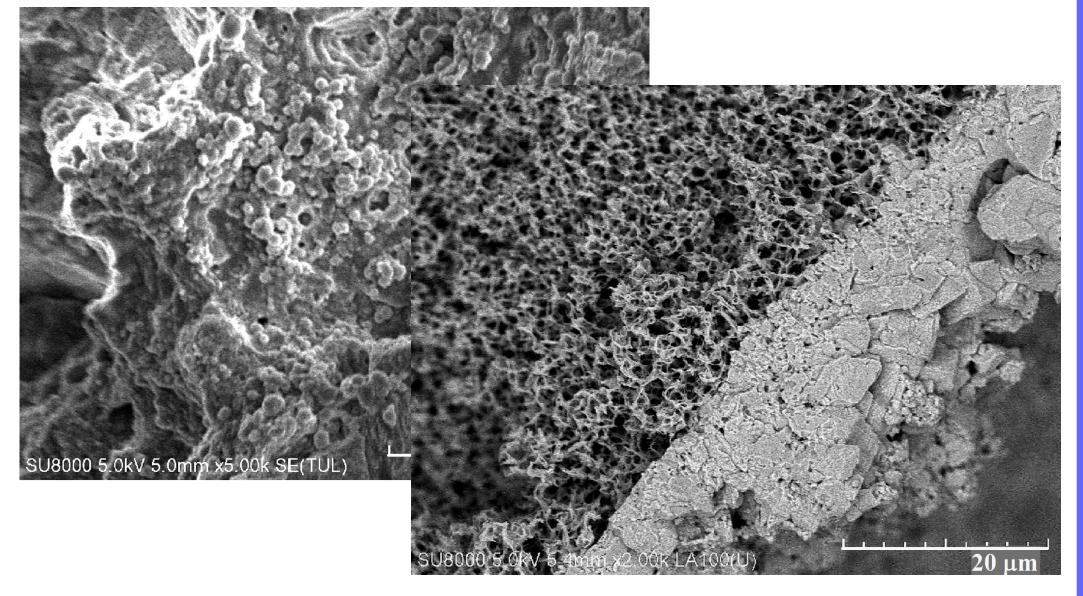


Fig. 2. Changes of the permeate flux and distillate electrical conductivity as a function of process time. ND –distillate tank refilled with distilled water. Feed: tap water (313 K).

Fig. 3. Changes of the permeate flux and distillate electrical conductivity as a function of process time. ND –distillate tank refilled with distilled water. Feed: tap water (333 K).

Fig. 4. Changes of ions concentration in the feed during MD process.





SU8000 5.0kV 8.0mm x5.00k SE(UL)

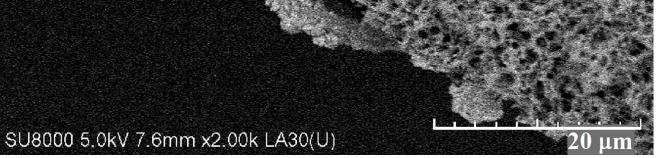


Fig. 5. SEM image of the membrane surface and cross-section (313 K)

Fig. 6. SEM image of the membrane surface and cross-section (333 K)

CONCLUSIONS

The used PP membranes exhibited a good resistance to wettability during a long-term study of water demineralization by MD process.

A lowering of the feed temperature to 313 K allowed to significantly limit the scaling intensity and as a result, the MD process can be operated for several months without necessity to clean the modules.

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